# 

## .. Thermodynamics

Only two independent variables  $\implies$  Maxwell and other Relations

Equation of state as a 2D surface in a non-Euclidean space

Second Law in terms of properties of the system: Potentials U,H,F,G

"Good Physicists Have Studied Under Very Fine Teachers"



Potentials: coefficients in opposite corners, differentials adjacent. Sign goes with coefficient. e.g. dF = -SdT - PdVMaxwell: Use corners, signs and constants from the bottom variables. e.g.  $\frac{dS}{-dP_T} = \frac{dV}{dT_P}$ 

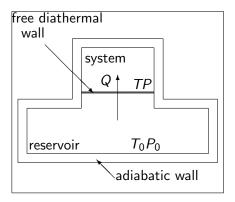


System in equilibrium with itself. Mechanical and Thermal Equilibrium... ... between any two parts. Pressure temperature "boundary" Consider a system held at  $T_0$ ,  $P_0$ , initially out of equilibrium. Heat flows, and work is done as it equilibrates.

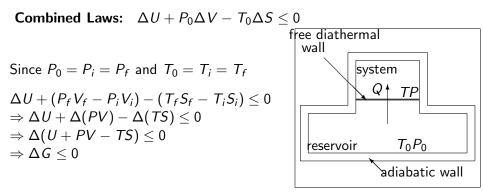
Change in surroundings  $\Delta S_0 = -Q/T_0$ ,  $\Delta V_0 = \Delta V = W/P_0$ 

Eventually system reaches equilibrium.

2nd law  $\Delta S_{sys} + \Delta S_0 \ge 0$ . 1st law  $Q = \Delta U + P_0 \Delta V$ Combined:  $\Delta U + P_0 \Delta V - T_0 \Delta S < 0$ 



## System goes to Equilibrium



Any change moving towards equilibrium must reduce  $G_{sys}$ Minimising  $G_{sys}$  is equivalent to maximising  $S_{sys} + S_0$ : i.e. obeys 2nd law.

## Evaluate $\left(\frac{\partial V}{\partial P}\right)_s$ ?

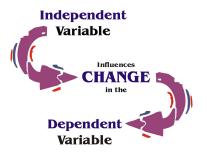


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- Compressibility of a particular substance?
- Half a Maxwell relation?
- Adiabatic change in volume as pressure increases?
- Something to do with Power and Voltage?



## Dependent and Independent Variables

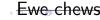




In thermodynamic derivations, it is not obvious what to choose as the dependent variable.

This is the *physics* of the question. The rest is just maths.





## Example: The difference in heat capacities, $C_P - C_V$

- What is the general relation between  $C_P$  and  $C_V$ ?
- $C_P C_V = nR$  is valid only for an Ideal gas
- Constant volume  $\implies$  no work. dU = TdS PdV = TdS

$$C_{V} = d^{2}Q_{V}/dT = \left(\frac{\partial U}{\partial T}\right)_{V} = T\left(\frac{\partial S}{\partial T}\right)_{V}$$

This suggests working with the entropy : S = S(T, V)

$$dS = \left(\frac{\partial S}{\partial T}\right)_{V} dT + \left(\frac{\partial S}{\partial V}\right)_{T} dV$$

For  $C_p = (\partial H / \partial T)_p = T (\partial S / \partial T)_p$ , differentiate wrt T at constant P.

$$C_P = T\left(\frac{\partial S}{\partial T}\right)_P = T\left(\frac{\partial S}{\partial T}\right)_V \left(\frac{\partial T}{\partial T}\right)_P + T\left(\frac{\partial S}{\partial V}\right)_T \left(\frac{\partial V}{\partial T}\right)_P$$

## Identify terms which are materials properties

$$C_{P} = T \left(\frac{\partial S}{\partial T}\right)_{V} + T \left(\frac{\partial S}{\partial V}\right)_{T} \left(\frac{\partial V}{\partial T}\right)_{P}$$

Introducing heat capacity

$$C_V = T \left(\frac{\partial S}{\partial T}\right)_V$$

and isobaric thermal expansivity:

$$\beta = \frac{1}{V} \left( \frac{\partial V}{\partial T} \right)_{P}$$
$$C_{P} - C_{V} = TV\beta \left( \frac{\partial S}{\partial V} \right)_{T}$$

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#### Eliminate the unmeasurable

$$C_P - C_V = TV\beta \left(\frac{\partial S}{\partial V}\right)_T$$

Recall S is not readily measurable, so use Maxwell to eliminate S.

$$\left(\frac{\partial S}{\partial V}\right)_{T} = \left(\frac{\partial P}{\partial T}\right)_{V} = -\left(\frac{\partial P}{\partial V}\right)_{T} \left(\frac{\partial V}{\partial T}\right)_{P}$$

and introduce the isothermal bulk modulus and thermal expansivity (again)

$$= -V\left(\frac{\partial P}{\partial V}\right)_{T}\frac{1}{V}\left(\frac{\partial V}{\partial T}\right)_{P} = \frac{1}{V}KV\beta = K\beta$$

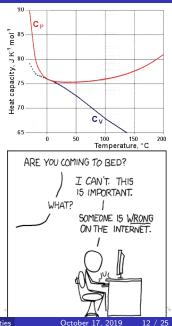
 $\mathcal{K} = -V\left(\frac{\partial P}{\partial V}\right)_T$  and  $\beta = \frac{1}{V}\left(\frac{\partial V}{\partial T}\right)_P$ 

$$C_P - C_V = TV\beta^2 K = TV\beta^2/\kappa$$

where  $\kappa = 1/K$  is the isothermal compressibility.

## Deconstruct $C_P - C_V = TV\beta^2 K = TV\beta^2/\kappa$

- $C_P C_V \propto V \implies$  extensive quantity.
- K is positive for all known substances.
- $\beta^2$  is positive.
- $C_P > C_V$ , even for negative thermal expansion.
- Difference is NOT due to work done expanding the material.
- $C_V = C_P$  at the density maximum in water.
- $\beta$  is small except for gases, so  $C_P \approx C_V$ .
- So for solids and liquids we often (lazily) just give "heat capacity"

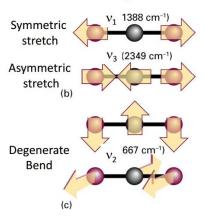


## Ways and heat capacities: $\hat{c}$



 $C_{p} - C_{y}$ 

γ



Gas	С <sub>и</sub> (J-К <sup>-1</sup> то	<i>C<sub>p</sub></i> ⊩¹)
Monatomic gas	ses	
He	12.5	20.8
Ar	12.5	20.8
Ne	12.7	20.8
Kr	12.3	20.8
Diatomic gases	s	
H <sub>2</sub> <sup>©</sup> Http:/	/miniph <sub>204</sub> ic	5 28.8
N2	20.8	29.1
0 <sub>2</sub>	21.1	29.4
cõ	21.0	29.3
CI	05.7	047

CO,

12.5	20.8	8.33	1.67
12.5	20.8	8.33	1.67
12.7	20.8	8.12	1.64
12.3	20.8	8.49	1.69
20.4	S 28.8	8.33	CO.41
20.8	29.1	8.33	1.40
21.1	29.4	8.33	1.40
21.0	29.3	8.33	1.40
25.7	34.7	8.96	1.35
28.5	37.0	8.50	1.30
32.4	40.4	9.00	1.29
27.0	35.4	8.37	1.30
	12.5 12.7 12.3 <b>p</b> 20.4 20.8 21.1 21.0 25.7 28.5 32.4	12.5 20.8 12.7 20.8 12.3 20.8 <b>ph20.4 CS 28.8</b> 20.8 29.1 21.1 29.4 21.0 29.3 25.7 34.7 28.5 37.0 32.4 40.4	12.5 20.8 8.33   12.7 20.8 8.12   12.3 20.8 8.49   p120.4 S.28.8 S.33   20.8 29.1 8.33   21.1 29.4 8.33   21.0 29.3 8.33   25.7 34.7 8.96   28.5 37.0 8.50   32.4 40.4 9.00

Entropy and heat capacity depend on how may degrees of freedom are available for heat.  $1000 \text{ cm}^{-1} = 1439 \text{K}$ : Not active at room temperature!

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Lecture 9: Relationships between properties

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## Variations in $C_V$ and $C_P$ (Third derivatives)

What is 
$$\left(\frac{\partial C_V}{\partial V}\right)_T$$
?

$$\begin{pmatrix} \frac{\partial C_V}{\partial V} \end{pmatrix}_T = T \left( \frac{\partial}{\partial V} \left( \frac{\partial S}{\partial T} \right)_V \right)_T = T \left( \frac{\partial}{\partial T} \left( \frac{\partial S}{\partial V} \right)_T \right)_V$$
$$= T \left( \frac{\partial}{\partial T} \left( \frac{\partial P}{\partial T} \right)_V \right)_V = T \left( \frac{\partial^2 P}{\partial T^2} \right)_V$$

using a Maxwell relation. An analogous analysis for  $C_P$  yields

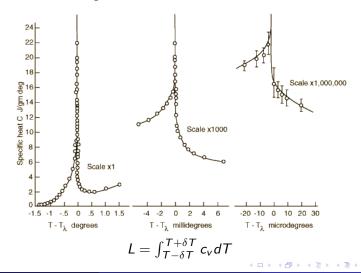
$$\left(\frac{\partial C_P}{\partial P}\right)_T = -T \left(\frac{\partial^2 V}{\partial T^2}\right)_P$$

 $\hat{C}_{V}$  derivatives come directly from equation of state! e.g.  $\left(\frac{\partial C_{P}}{\partial P}\right)_{T} = 0$  for Ideal Gas V=RT/P. (regardless of monatomic/diatomic etc.)

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#### Aside: Latent heats and the Lambda Function

Formally,  $c_P$  is infinite at a phase transition ( $\Delta V \neq 0$ ,  $\Delta T = 0$ ). e.g. liquid He: the integral under the delta-function is the Latent Heat.



Relate the volume and pressure derivatives of the internal energy to material properties and gradients of equation of state. Differentiate dU = TdS - PdV, wrt dV and eliminate S using a Maxwell relation:

$$\left(\frac{\partial U}{\partial V}\right)_{T} = T\left(\frac{\partial S}{\partial V}\right)_{T} - P = T\left(\frac{\partial P}{\partial T}\right)_{V} - P = \frac{T\beta}{\kappa} - P$$

Is force the derivative of energy? Compare  $F = -\nabla U$ ,  $P = -\left(\frac{\partial U}{\partial V}\right)_S$ 

Similarly, differentiate dU = TdS - PdV, wrt dP and eliminate S using a Maxwell relation:

$$\left(\frac{\partial U}{\partial P}\right)_{T} = -T\left(\frac{\partial V}{\partial T}\right)_{P} - P\left(\frac{\partial V}{\partial P}\right)_{T} = -TV\beta + PV\kappa_{T}$$

In the tutorial you will show

$$\frac{C_P}{C_V} = \frac{\kappa_T}{\kappa_S}$$

where  $\kappa_T$  and  $\kappa_S$  are the isothermal and adiabatic compressibilities:

$$\kappa_T = -\frac{1}{V} \left( \frac{\partial V}{\partial P} \right)_T$$
 and  $\kappa_S = -\frac{1}{V} \left( \frac{\partial V}{\partial P} \right)_S$ 

Another link between thermal and mechanical properties of materials.

#### The entropy of an ideal gas, again

For entropy per mole s = s(T, V), we can always write

$$ds = \left(\frac{\partial s}{\partial T}\right)_{V} dT + \left(\frac{\partial s}{\partial v}\right)_{T} dV = c_{V} \frac{dT}{T} + \beta K dV$$

This equation applies to any fluid.  $\beta$  is thermal expansivity, K bulk modulus.

For an Ideal gas  $\beta K = R/v$  and  $c_v$  is a constant. Integration then gives

$$s = c_v \ln T + R \ln v + s_0$$

Similarly  $s = c_P \ln T - R \ln P + s_0$ .

Again, we relate *changes* in entropy to measurable quantities via the equation of state.

## Availability



1904 Prince Piero Ginori Conti. generating electric energy from geothermal steam

- How much work can be extracted from a system?
- Depends on surroundings, but how?

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## Availability - non Infinite reservoirs

Second-law for system with surrounding reservoir at  $T_0$ ,  $P_0$ 

$$\Delta S + \Delta S_{surr} \geq 0 \ \Delta S - rac{Q}{T_0} \geq 0$$

Q is heat transferred from the reservoir into the system. First law for system gives  $Q = \Delta U + P_0 \Delta V$ :

$$\Delta U + P_0 \Delta V - T_0 \Delta S \leq 0$$

Define a new function called the Availability, A,

$$A = U - T_0 S + P_0 V$$

- Availability is **not** Gibbs free energy.
- Depends on both the system and surroundings.  $A(S, V, P_0, T_0)$ ,
- Spontaneous changes in availability are always negative  $\Delta A = \Delta U T_0 \Delta S + P_0 \Delta V \le 0$
- At equilibrium, nothing more can change: Availability is minimised

$$dA = dU - T_0 dS + P_0 dV = 0$$

At equilibrium  $(T = T_0, P = P_0), dA = 0$ 

If $T = T_0$	&	$P = P_0$	A = U - TS + PV		G is minimum
If $T = T_0$	&	V = const	A = U - TS + const	<i>.</i> .	F is minimum
If S is const.	&	V = const	A = U + const	<i>.</i> .	U is minimum
If S is const.	&	$P = P_0$	A = U - const + PV		H is minimum
If $U$ is const.	&	V = const	$A = const - T_0S$		S is maximum

- Minimising Availability maximises entropy of the Universe.
- Availability is minimised when system is in equilibrium with surroundings.
- Availability tells us how far from equilibrium we are

The work  $P_0\Delta V$ , is used to push back the environment. The heat transfer could run an engine producing *useful work*.

$$\Delta U = Q - W = Q - W^{useful} - P_0 \Delta V \tag{1}$$

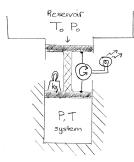
where Q is the heat transported from the surroundings to the system,

$$\Delta U + P_0 \Delta V - T_0 \Delta S + W^{useful} = W^{useful} - \Delta A \le 0$$

Maximum useful work is  $W_{max} = -\Delta A$ . (iff all changes are reversible). Likewise, with a small differential change of A:

$$dW_{useful} \leq -dA = -dU + T_0 dS - P_0 dV$$
$$= (T_0 - T)dS + (P - P_0)dV$$

## Available for work





$$dW_{useful} \leq (T_0 - T)dS + (P - P_0)dV$$

Useful work could come from

- moving entropy (heat) from hot body (T) to cold body (T<sub>0</sub>).
- pushing a piston against a pressure  $(P_0)$

Once the availability is used up - no more work.

n.b. the system T changes as it equilibrates

Idealised engines had two infinite T-reservoirs, hot and cold.

Real engines need continual supply of energy to maintain the temperatures.